

# Effects of Buffering and Urea on the Quantity and Quality of Biogas From Banana Leaves as Alternative Renewable Energy Resource.

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## Abstract

Buffer solutions of different molar concentrations (0.1M, 0.2M, 0.3M, .4M and 0.5M) were prepared using buffer salts ( $\text{Na}_2\text{HPO}_4$  and  $\text{NaH}_2\text{PO}_4 \cdot \text{H}_2\text{O}$ ). The pKa of the buffer salts was determined from the ionization constant,  $K_a$  ( $7 \times 10^{-8}$ ) of the phosphoric ions ( $\text{HPO}_4^{2-}$  and  $\text{H}_2\text{PO}_4^-$ ) of the buffer salts using the relation,  $\text{pKa} = -\log K_a$ . The pKa of the buffer salts obtained was further used in Henderson-Hasselbalch's equation,  $\text{pH} = \text{pKa} + \log [\text{base}]/[\text{acid}]$ , where the volumes ( $125\text{cm}^3$  each) of the prepared buffer solution of required pH (6.8, 7.0, 7.2, 7.4 and 7.6) were prepared. Slurries were prepared using 20g banana leaves in  $125\text{cm}^3$  of the prepared buffer solutions. For the investigation of the effect of buffering on biogas yield and its composition, 0.1M, 0.2M, 0.3M, 0.4M and 0.5M buffer solutions (pH 7.0 each) were used in making the slurry; for the investigation of the effect of pH of buffer solution on the quantity and composition of biogas, buffer solutions of pH (6.8, 7.0, 7.2, 7.4 and 7.6) were separately used in making the slurry; for the investigation of the effect of addition of urea (as nutritive additive), 0.1g, 0.15g, 0.20g, 0.25g and 0.30g of urea, were respectively added into the five (5) replica slurries prepared from 20g banana leaves and  $125\text{cm}^3$  distilled water, which were labeled A,B,C, D and E and; for the investigation of the combined effect of buffering and addition of urea, 0.1g, 0.15g, 0.20g, 0.25g and 0.30g of urea (as additive), were respectively added into another five (5) replica slurries prepared from 20g banana leaves and  $125\text{cm}^3$  of 0.2M buffer solutions of pH 7.4, which were also labeled A,B,C,D and E. Compositional analysis of the biogas produced was also carried out by passing the gas collected (biogas) through concentrated NaOH solution (10M) and a solution of  $(\text{CH}_3\text{COO})_2\text{Pb}$  in a 3 molar  $\text{CH}_3\text{COOH}$ , where  $\text{CO}_2$  and  $\text{H}_2\text{S}$  were, respectively absorbed from the biogas. The work revealed that, the use of buffer solution at certain molar concentrations (0.1M – 0.3M) and pH (7.0 – 7.4); the use of urea ( $0.1\text{g}/125\text{cm}^3 - 0.25\text{g}/125\text{cm}^3$ ) equivalent to  $0.8\text{g}/\text{dm}^3 - 2.0\text{g}/\text{dm}^3$  and; the use of the combination of buffer solution and urea, each enhanced biogas yield. The compositional analysis carried out, revealed that the biogas (secondary biofuel) produced was of good fuel value (60 – 68.78%  $\text{CH}_4$ ) and low environmental hazards ( $\text{CO}_2$  below 40% and  $\text{H}_2\text{S}$  below 0.5%).

**Keywords:** Biogas; buffer solution; urea; molar concentration; ionization constant (pKa) of phosphoric ions; pH of slurry.

## 1. Introduction

The awareness of the imminent depletion of fossil fuels coupled with the global energy crisis all over the world has stimulated interest in the search for alternative energy sources. The potential alternative energy sources which have received much attention all over the world nowadays are water current, wind power, geothermal power, nuclear power, solar energy and organic wastes as pointed out by Garba *et al* (1996). Naturally, each of these has its own shortcomings, but solar energy and organic wastes are the most reliable alternative source of energy for third world countries (Nigeria inclusive) because they are by far more readily accessible to inhabitants of rural areas from the available biomass resources in their immediate environment.

Biomass has been defined as the natural biological storage of energy (Solar) and other materials in complex organic substances primarily by gross photosynthesis as reported by Zuru *et al* (2001). The biomass resources of Nigeria are wood, forage grasses and shrubs, human and animal excretion, aquatic biomass and wastes arising from forestry and, agricultural, municipal and industrial activities. The biomass reserve of Nigeria has been estimated at about  $9.0 \times 10^2$  MJ as reported by Garba (1998) while the total world mass of forest is put at 1,600 billion tones as reported by Ramage & Seurlock (1990). When biomass are used directly for energy, they are called primary biofuels. On the other hand, if the biomass resources are converted to fuels through bioconversion processes, the derived fuels (biogas, ethanol e.t.c) are referred to as secondary biofuels as explained by Loughton (1990). The inefficient use of primary biofuels in most developing countries (Nigeria inclusive) has caused many ecological problems such as deforestation, desertification, erosion and reduced biodiversity as reported by Kgbathi(1997). Moreover, the adverse health problems associated with the indoor pollution from biomass use (as primary biofuel) include respiratory diseases chronic lung diseases and cancer as report by Smith (1991). Thus, the used to develop efficient methods of using the available biomass resources in our environment for fuel

generation is imperative. Fortunately, the use of secondary biofuels has proved more efficient with biogas emerging as the most attractive option nowadays. Unfortunately, the actual biogas yield from biomass resources through bioconversion process is much lower than expected, the shortfall is attributed to the inadequate supply of minerals nutrients among other factors required by the micro-organisms to grow, multiply and efficiently act on the substrate feedstock for biogas production as explained by Zuru *et al* (1997). For this reason, attempts to improve the biogas yield from biomass resources of different origin (plants and animals) through bioconversion process have been made. For instance, Guiot *et al* (1988), have reported improved growth of methanogens due to the supply of appropriate mixture of  $\text{Ni}^{2+}$ ,  $\text{Co}^{2+}$  and  $\text{Mo}^{6+}$  Singh *et al* (1992), added different concentrations of  $\text{Na}^+$ ,  $\text{Mg}^{2+}$ ,  $\text{Fe}^{2+}$ ,  $\text{Al}^{3+}$ ,  $\text{Sn}^{2+}$  and  $\text{Cd}^{2+}$  salts into the slurry of *Ecphoria crissipes* and investigated the effects of these salts on the cumulative gas yield of the substrate. They found that,  $\text{Na}^+$  and  $\text{Al}^{3+}$  salts had no adverse effect at low concentration but caused a significant increase in gas production rate at concentration above 500mg/kg of waste;  $\text{Fe}^{2+}$ ,  $\text{Mg}^{2+}$  and  $\text{Cd}^{2+}$  showed inhibitory effects and;  $\text{Sn}^{2+}$  stopped the gas production completely. Machido *et al* (1996), investigated the effect of  $\text{Ca}^{2+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Mo}^{6+}$ ,  $\text{Co}^{2+}$  and  $\text{B}^{3+}$  ions on the production of biogas from cow dung slurry. They observed that, the gas yielded in the digesters containing  $\text{Ca}^{2+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Mo}^{6+}$ ,  $\text{Co}^{2+}$  and  $\text{B}^{3+}$  were 3.44%, 1.72%, 1.72%, 8.34% and 7.14%, respectively of that yielded by the control digester. Similarly, Zuru *et al* (1997), studied the effect of addition of Ca, B and Co salts on biogas production from cow dung. The work revealed that the salts added had neither inhibitory nor enhancing effect on the total gas yield, but they stimulated early gas production. In addition to the aforementioned efforts and many others made by different researches towards promoting biogas production from different substrates, this research is aimed at investigating the influence of buffer solution and urea on the quantity and composition of biogas (secondary biofuel) from banana leaves as alternative and environmentally – friendly renewable energy resource.

## 2. Materials and Methods

### 2.1 Chemical/Reagents

The chemicals/reagents used for this research were disodium hydrogen phosphate ( $\text{Na}_2\text{HPO}_4$ ), ethanoic acid ( $\text{CH}_3\text{COOH}$ ), lead ethanoate  $\{(\text{CH}_3\text{COO})_2\text{Pb}\}$ , Sodium dihydrogen phosphate monohydrate ( $\text{NaH}_2\text{PO}_4 \cdot \text{H}_2\text{O}$ ), Sodium hydroxide ( $\text{NaOH}$ ) and urea ( $\text{CO}(\text{NH}_2)_2$ ). The chemicals/reagents were general purpose reagents of good analytical grade, products of BDH Chemicals LTD, Poole-England.

### 2.2 Apparatus

The apparatus used were the common laboratory glass wares, electric beam balance, mesh, oven, pestle and mortar pH metre, PVC tube and stirrer.

### 2.3 Sample Collection and Treatment

The banana leaves were collected from a group of banana plants planted by Kano Agricultural and Rural Development Authority (KNARDA) in Bichi town, Kano State – Nigeria. The banana leaves were fresh and mature at the time of collection. The sample (banana leaves) was oven-dried at  $37^\circ\text{C}$  for four (4) hours ground using pestle and mortar and sieved to a mesh size less than  $250\mu\text{m}$  using mesh of a well defined porosities for different particles sizes.

### 2.4 Preparation of Reactants (Slurries)

The slurry used in the control digester was prepared by dissolving 20g of the treated sample with  $125\text{cm}^3$  distilled water in a reactor ( $250\text{cm}^3$  Buchner flask) and thoroughly stirred for homogeneity. The pH of the slurry was measured using pH metre. For the preparation of slurry using buffer solution, the pKa of the buffer salts was first determined using the relation,  $\text{pKa} = -\log \text{Ka}$ . The determined pKa was further used in Henderson Hesselbalch equation,  $\text{pH} = \text{pKa} + \log [\text{conjugate base}]/[\text{acid}]$ , from which the volumes of the buffer salts (acid and base) that were mixed and formed a buffer solution of required molar concentration and pH (See Appendix I). The slurry was prepared by dissolving 20g of the treated (prepared) sample and 0.9g of yeast in  $125\text{cm}^3$  of the prepared buffer solution in  $250\text{cm}^3$  Buchner flask. For the investigation of the effect of concentration of buffer solution on biogas yield and its composition, different molar concentrations (0.1M, 0.2M, 0.3M, 0.4M and 0.5M) of buffer solution of equal pH (7.0) were used in making the slurry. For the investigation of the effect of pH of buffer solution on the quantity and composition of biogas, different pH (6.8, 7.0, 7.2, 7.4 and 7.6) of buffer solution were used in making the slurry. In order to investigate the effect of urea on the quantity and composition of biogas, a slurry was prepared by dissolving 20g of the prepared sample in  $125\text{cm}^3$  distilled water in a reactor ( $250\text{cm}^3$  Buchner flask). Five (5) replica slurries were prepared into which 0.1g, 0.15g, 0.20g, 0.25g and 0.30g of urea, were respectively added. For the investigation of the combined effect of buffering and addition of urea on the quantity and composition of biogas, a slurry was prepared by dissolving 20g of the prepared sample in  $125\text{cm}^3$  of 0.2M buffer solution (pH 7.4) and placed into a reactor ( $250\text{cm}^3$  Buchner flask). Five (5) replica slurries were also prepared into which 0.10g, 0.5g, 0.20g, 0.25g and 3.0g of urea were respectively added. The reactors ( $250\text{cm}^3$  Buchner flasks) into which the prepared slurries were placed for each of the investigations (effect of buffering, effect of urea and the combined effect of buffering and urea) were

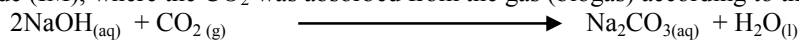
labeled A, B, C, D and E and each was connected to a gas collecting apparatus (an inverted 500cm<sup>3</sup> measuring cylinder filled with brine) using a PVC rubber tube (50cm long and 8.5cm internal diameter), which was positioned up right in the measuring cylinder. The digesters were made in duplicate.

### 2.5 Experimental Set up

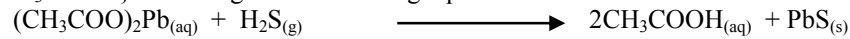
The digesters were made air-tight according to the procedure described by Uba & Garba (2001). The digesters were immersed about 1/3 in water bath operated at 33°C and, the degradation process was allowed to continue for 15 days according to the degradation method adopted by Yaro (2011) with few adjustment in the quantity of the slurry, size of the digester and duration of the reaction. The collection of the gaseous degradation product (biogas) was carried out according to the collection method adopted by Gumel & Yaro (2012). The volume of the gas collected from each digester was measured by water displacement method as described by Ekwenchi & Yaro (2010). The mean (average) volume of gas collected from each digester was evaluated and recorded at fixed daily intervals for 15 consecutive days.

### 2.6 Evaluation Procedure

In order to evaluate the composition of the biogas generated, the techniques adopted by Yaro (2011) were used. The carbon (IV) oxide (CO<sub>2</sub>) content of the biogas was removed by passing through concentrated Sodium hydroxide (IM), where the CO<sub>2</sub> was absorbed from the gas (biogas) according to the following equation:



The H<sub>2</sub>S content of gas was removed by absorption using lead ethanoate solution in 3M ethanoic acid {(CH<sub>3</sub>COO)<sub>2</sub>Pb/CH<sub>3</sub>COOH} according to the following equation:



The percentages of the secondary biofuel (CH<sub>4</sub>), CO<sub>2</sub> and H<sub>2</sub>S in the biogas were evaluated as follows:

$$\begin{aligned} \% \text{CO}_2 &= \frac{V_{\text{CO}_2}}{V_{\text{biogas}}} \times 100 \\ \% \text{H}_2\text{S} &= \frac{V_{\text{H}_2\text{S}}}{V_{\text{biogas}}} \times 100 \\ \% \text{CH}_4 &= \frac{V_{\text{biogas}} - (V_{\text{CO}_2} + V_{\text{H}_2\text{S}})}{V_{\text{biogas}}} \times 100 \\ \text{Where } V &= \text{Volume (cm}^3\text{)} \end{aligned}$$

## 3. Results

The results of all the investigations carried out are shown in Tables 1, 2, 3 and 4 below:

Table 1, 2 and 3 show the mean total volumes of biogas (cm<sup>3</sup>) collected, from 20g of banana leaves, which were anaerobically digested at 33°C over a period of 15 consecutive days under the influence of the concentration of buffer solution, pH of buffer solution and addition of urea, respectively. Table 4 shows the quantity and composition of biogas generated through anaerobic fungal degradation of 20g of banana leaves at 33°C for 15 consecutive days under the combined influence of buffer solution and urea.

## 4. Discussion

The results of the effects of concentration of buffer solution, pH of buffer solution, addition of urea and the combination of buffer solution and urea are shown in Tables 1, 2, 3 and 4, respectively.

From the results (Table 1 and 2), it could be seen that, at certain ranges of concentration (0.1M – 0.3M) and pH (7.0 – 7.4) of buffer solution, there was remarkable increase in gas production when compared with the control digester in which distilled water was used. The increase in gas production may be attributed to the presence of Na<sup>+</sup> and P<sup>-5</sup> in the buffer salts, which served as inorganic nutrients (fertilizers) for the fermentative bacteria and stimulated their growth and activities. This is accordance with the findings of Singh *et al* (1992) & Airehrour (1994). The increase could also be attributed to favourable conditions (in terms of suitable pH) into which the fermentative microbes were rendered. This is because fermentative microbes require a neutral or mildly alkaline environment for their proper growth and metabolic activities as pointed out by Ariane (1985). On the other hand, the use of buffer solution (in terms of both the effects of concentration and pH) each brought about a slight decrease in the percentage of CH<sub>4</sub> (secondary biofuel) content of the biogas and a slight increase in the percentages of CO<sub>2</sub> and H<sub>2</sub>S (associated contaminants of the secondary biofuel). The increase in CO<sub>2</sub> may be connected to the oxidation of carbon content of the substrate by the oxygen content of the buffer salt as pointed out by Gumel & Yaro (2012) while the increase in H<sub>2</sub>S may be associated with the drastic degradation of sulphur containing amino acids and proteins content of the substrate, as pointed out by Harrison & de Mora (1996). The increase in H<sub>2</sub>S may also be associated with the reduction of sulphate ion (SO<sub>4</sub><sup>2-</sup>) mediated by sulphur containing compounds in the substrate feedstock as reported Ahmad (2000). The changes in the percentage composition of the biogas has no significant impact on the good fuel quality of the secondary biofuel formed. This is because the percentage of CH<sub>4</sub> in the biogas is still up to 60 and, that of CO<sub>2</sub> is below 40 and, for a biogas be of good fuel

value (high calorific value) and low environmental hazards, the CH<sub>4</sub> content must exceed 60% and, the CO<sub>2</sub> content below 40% as pointed out by Ekwenchi & Yaro (2010).

From Table 3, it could be seen that addition of urea at a certain range of mass concentration (0.1g/125cm<sup>3</sup> – 0.25g/125cm<sup>3</sup>) enhanced biogas generation. The enhancing effect of urea on biogas yield may be connected to the fact that urea contains elements needed for fungal (bacteria) growth for instance, the presence of amine (-NH<sub>2</sub>) in the urea serves as source of nitrogen (N), which is needed by the fermentative microbes for their growth as pointed out by Garba (1988) while the presence of Ketone (>C=O) serves as source of carbon (C), which is required by the fermentative microbes for energy supply and generation of secondary biofuel (CH<sub>4</sub>) from substrate feedstock as pointed out by Obinwanne (1999). The effect of urea on the composition of biogas also caused in a slight decrease in CH<sub>4</sub> and an increase (slightly) in CO<sub>2</sub> and H<sub>2</sub>S. The slight increase in CO<sub>2</sub> content of the biogas observed may be attributed to the release of CO<sub>2</sub> during the hydrolysis of urea in the slurry. This is in line with the statement of Murry (1977), which says that, urea hydrolyses in the presence of enzyme (urease) and yields CO<sub>2</sub>. The increase in CO<sub>2</sub> could also be associated with the formation of H<sub>2</sub>CO<sub>3</sub> from hydrolysis of urea, which decomposes instantaneously to CO<sub>2</sub> and H<sub>2</sub>O as pointed out by Yaro (2011). The increase in H<sub>2</sub>S content of the biogas due to the addition of urea may be attributed to drastic degradation of sulphur containing compounds in the substrate feedstock by the fermentative fungi as reported by Harrison and de Mora (1996). Just like in the case of the effect of buffering, addition of urea has no significant effect on the quantity of the biogas produced (as fuel) because the CH<sub>4</sub> content of the biogas was above 60%, with CO<sub>2</sub> content below 40%.

Table 4 showed that the use of the combination of buffer solution and urea at certain concentration and pH greatly enhanced biogas generation with significant change in composition of the biogas when compared with the respective effects of buffering and addition of urea separately (when they are not combined). The relative increase in the quantity of biogas observed due to the collective effect of buffering capacity and addition of urea was connected to the presence of Na<sup>+</sup> and P<sup>5-</sup> ions in the buffer solution which served as fertilizers and, stimulated the growth and activities of the fermentative bacteria as reported by Singh *et al* (1992) & Airehvoir (1994); the presence of -NH<sub>2</sub> and >C=O groups in the fertilizer, which served as sources of nitrogen and carbon, respectively as pointed out by Obinwanne (1997) and; the favorable pH condition of the slurry as pointed out by Ariane (1985). On the other hand, the drastic change in the composition of biogas due to the combined effect of buffering and urea may be attributed to the chemical nature of the substrate feedstock, buffer solution and urea added. For instance, the increase in CO<sub>2</sub> may be connected to the: oxidation of carbon content of the substrate feedstock by the oxygen content of the buffer solution as pointed out by Gumel & Yaro (2012); hydrolysis of urea in the presence of enzyme (fermentative bacteria), which release CO<sub>2</sub> as pointed out by Murray (1977) and; decomposition of H<sub>2</sub>CO<sub>3</sub> formed during fermentation into CO<sub>2</sub> and H<sub>2</sub>O as pointed out by Yaro (2011). The increase in H<sub>2</sub>S may be connected to the degradation of sulphur containing amino acids and proteins in substrate feedstock as pointed by Harrison & de Mora (1996) and reduction of sulphate ion (SO<sub>4</sub><sup>2-</sup>) mediated by sulphur containing compounds as pointed out by Ahmad (2001). Of all the changes in the composition of the biogas, the biogas obtained was of good fuel value and low environmental hazards because the CH<sub>4</sub> content of the biogas was up to 60% and the CO<sub>2</sub> and H<sub>2</sub>S contents, were respectively below 40% and 0.15%.

## 5. Conclusion

From the quantity (681cm<sup>3</sup>) and the percentage composition of the biogas (60% CH<sub>4</sub>, 39.57% CO<sub>2</sub> and 0.43% H<sub>2</sub>S) generated under the collective influence of buffer solution and urea, it can be concluded that, the use of buffer solution and urea at certain ranges of concentration and pH level, enhances biogas generation with good fuel value and low environmental hazards from banana leaves.

## 6. Acknowledgement

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Table 1: Effect of Concentration of Buffer Solution (pH 7.0) on the Quantity and Composition of Biogas Produced Over a Period of 15 Days.

Digester	Conc. of Buffer solution	Biogas yield (cm <sup>3</sup> )	% Composition of biogas		
			CH <sub>4</sub>	CO <sub>2</sub>	H <sub>2</sub> S
A	0.10	440.00	64.82	35.00	0.18
B	0.20	546.00	64.81	35.00	0.19
C	0.30	432.50	64.81	35.01	0.18
D	0.40	315.00	64.80	35.02	0.18
E	0.50	224.50	64.82	35.00	0.18
Control	Distilled water (pH 6.90)	365.00	68.78	31.10	0.12

\*Key: Conc.= concentration

Table 2: Effect of pH of 0.2m Buffer Solution (pH 7.2) on the Quantity and Composition of Biogas Produced Over a Period of 15 Days.

Digester	pH of buffer solution	Biogas yield (cm <sup>3</sup> )	% Composition of Biogas		
			CH <sub>4</sub>	CO <sub>2</sub>	H <sub>2</sub> S
A	6.80	320.00	64.80	35.01	0.19
B	7.00	545.00	64.80	35.00	0.20
C	7.20	562.50	64.82	35.00	0.18
D	7.40	635.00	64.80	35.01	0.19
E	7.60	349.50	64.81	35.00	0.19
Control Distilled water (pH 6.90)		365.00	68.78	31.10	0.12

Table 3: Effect of Urea on the Quantity and Composition of Biogas Produced Over a Period of 15 Days.

Digester	Urea added (g)	pH of the slurry	Biogas yield (cm <sup>3</sup> )	% Composition of Biogas		
				CH <sub>4</sub>	CO <sub>2</sub>	H <sub>2</sub> S
A	0.1	7.10	460.00	63.98	35.19	0.35
B	0.15	7.30	582.00	63.98	35.68	0.34
C	0.20	7.40	595.00	63.87	35.77	0.34
D	0.25	7.50	456.00	63.97	35.69	0.34
E	0.30	7.80	322.00	63.85	35.79	0.36
Control	0.00	6.90	365.00	68.78	31.10	0.12

Table 4: Combined Effects of 0.2M Buffer Solution (pH 7.4) and Urea on the Quantity and Composition of Biogas Produced Over a Period of 15 Days.

Digester	Urea added (g)	pH of the slurry	Biogas yield (cm <sup>3</sup> )	% Composition of Biogas		
				CH <sub>4</sub>	CO <sub>2</sub>	H <sub>2</sub> S
A	0.10	7.60	473.00	59.94	39.63	0.43
B	0.15	78.0	632.00	60.00	39.58	0.42
C	0.20	7.90	681.00	60.01	39.57	0.42
D	0.25	8.20	402.00	60.00	39.56	0.44
E	0.30	8.20	206.00	59.95	39.62	0.43
Control	0.00	6.90	365.00	68.78	31.10	0.12

## APPENDIX: PREPARATION OF BUFFER SOLUTION

**Appendix I:** Preparation of 0.1M Buffer Solution (pH 7.0) Using Buffer Salts (NaH<sub>2</sub>PO<sub>4</sub>·H<sub>2</sub>O and Na<sub>2</sub>HPO<sub>4</sub>) of Ionization Constant (K<sub>a</sub>) = 7 x 10<sup>-8</sup>.

The pK<sub>a</sub> of the buffer salts was evaluated from the given K<sub>a</sub> as follows:

$$\text{pKa} = -\text{Log Ka} \quad \text{_____} \quad (1)$$

$$\Rightarrow \text{pKa} = -\log 7 \times 10^{-8}$$

$$= -(-7.1549)$$

$$= 7.1549 \approx 7.155 \quad \text{_____} \quad (2)$$

The volumes of acid (V<sub>a</sub>) and the volume of base (V<sub>b</sub>) were obtained using Henderson-Hasselbelch's equation as follows:

$$\text{pH} = \text{pKa} + \text{Log}_{10} \left[ \frac{\text{conjugate base}}{\text{acid}} \right] \quad \text{_____} \quad (3)$$

Since pH of the buffer salts = 7.0, equation (3) becomes:

$$7.0 - 7.155 + \text{Log}_{10} \left[ \frac{[\text{HPO}_4^{2-}]}{[\text{H}_2\text{PO}_4^-]} \right]$$

$$-0.155 + \text{Log}_{10} \frac{[\text{HPO}_4^{2-}]}{[\text{H}_2\text{PO}_4^-]} \quad (4)$$

By inverting the R.H. S of equation (4), we have

$$0.155 = \text{Log}_{10} \frac{[\text{H}_2\text{PO}_4^-]}{[\text{HPO}_4^{2-}]}$$

$$\Rightarrow \text{Log}_{10} \frac{[\text{H}_2\text{PO}_4^-]}{[\text{HPO}_4^{2-}]} = 0.155$$

$$\Rightarrow \frac{[\text{H}_2\text{PO}_4^-]}{[\text{HPO}_4^{2-}]} = 10^{0.155}$$

$$\Rightarrow \frac{[\text{H}_2\text{PO}_4^-]}{[\text{HPO}_4^{2-}]} = 1.43 \quad (5)$$

But the mole ratio  $\frac{\text{acid}}{\text{Base}}$  is given by  $\frac{M_a V_a}{M_b V_b}$

$$\therefore \Rightarrow \frac{[\text{H}_2\text{PO}_4^-]}{[\text{HPO}_4^{2-}]} = \frac{M_a V_a}{M_b V_b} \quad (6)$$

By putting eqn. (5) into Eqn. (6), eqn. (6) becomes

$$\frac{M_a V_a}{M_b V_b} = 1.43 \quad (7)$$

But for buffer solution, the molar concentration of acid must be equal to the molar concentration of base (i.e.  $M_a = M_b$ ). For this reason, equation (7) becomes.

$$\frac{V_a}{V_b} = 1.43$$

$$\begin{aligned} \Rightarrow V_a &= V_b \times 1.43 \\ \Rightarrow V_a &= 1.43 V_b \quad (8) \end{aligned}$$

Since the volume of buffer solution used in preparing the slurry was  $125\text{cm}^3$ ,

$$\Rightarrow V_a + V_b = 125\text{cm}^3 \quad (9)$$

By substituting the value of  $V_a$  from eqn. (8) into Eqn. (9), eqn. (9) becomes.

$$\begin{aligned} 1.43V_b + V_b &= 125\text{cm}^3 \\ 2.43V_b &= 125\text{cm}^3 \\ \therefore V_b &= \frac{125\text{cm}^3}{2.43} \\ V_b &= 51.44\text{cm}^3 \quad (10) \end{aligned}$$

From eqn. (9),  $V_a + V_b = 125\text{cm}^3$

$$\begin{aligned} \therefore V_a &= 125\text{cm}^3 - 51.44\text{cm}^3 \\ &= 73.56\text{cm}^3 \quad (11) \end{aligned}$$

From eqns.(10) and (11), respectively  $51.44\text{cm}^3$  of base ( $\text{NaHPO}_4$ ) and  $73.56\text{cm}^3$  of acid ( $\text{Na}_2\text{HPO}_4 \cdot \text{H}_2\text{O}$ ), were respectively mixed and formed  $125\text{cm}^3$  of buffer solution (pH 7.0).

The same procedure was followed for determination of the volumes of acid ( $V_a$ ) and volumes of based ( $V_b$ ) for other molar concentrations (i.e. 0.2, 0.3, 0.4 and 0.5) and pH (6.8, 7.2, 7.4 and 7.6) of the buffer solution used.

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