

Advancement of A Lab-Scale Anaerobic Biodigester to Implement Monitoring and Sensing Technologies: A Promising Educational Instrument for Reducing Carbon Emissions and Combating Climate Change

Okafor, M.C.¹, Suleiman I.A.², Sekiteri P. A.³

1. Department of Civil Engineering Technology, School of Engineering, Auchi Polytechnic, Auchi, PMB 13, Auchi, Edo State

2. Department of Agricultural & Bioenvironmental Engineering, School of Engineering, Auchi Polytechnic, Auchi, PMB 13, Auchi, Edo State

3. Department of Mechanical Engineering, School of Engineering, Auchi Polytechnic, Auchi, PMB 13, Auchi, Edo State

Correspondence: suleiman_ibrahim@auchipoly.edu.ng

Abstract

This study showcases a laboratory-scale anaerobic biodigester designed to introduce monitoring and sensing methods for tracking microorganism growth based on various parameters, including redox potential, pH, pressure, and temperature, measured in a near-continuous manner. A microcontroller system (Atmega328—Arduino) was employed for this purpose. The design's foundation lies in flexible and open-source software, hardware, and firmware (Scilab, Arduino, Processing), making it easily adaptable for other relevant research. The biodigester was developed as an educational tool for engineering students to gain a deeper understanding of its operation and to track the system's properties and progression over time. This enables the creation of property curves, which can be correlated for a more comprehensive understanding of biodigester functionality. The study specifically explored the connection between the oxidation-reduction reaction and microbial activity, demonstrating that redox potential can effectively measure microorganism growth in an anaerobic environment. Ultimately, this laboratory-scale biodigester serves as an introduction to the technology typically utilised for controlling carbon footprints, particularly in the wastewater sector, and consequently contributes to climate change mitigation efforts.

Keywords: wastewater; low-carbon; biodigester; laboratory scale; open-source tools

DOI: 10.7176/JNSR/14-8-04

Publication date: May 31st 2023

Introduction

Anaerobic digestion technologies employed in organic wastewater treatment offer effective solutions to environmental issues while simultaneously generating energy. These sustainable, safe, and efficient biotechnologies contribute to carbon footprint reduction through methane capture and fossil fuel replacement [1–7]. While the process of anaerobic digestion has been utilised since ancient times, the focus has been on its final products rather than its underlying processes [3]. The adaptability of anaerobic digestion has made it a valuable technology for addressing key challenges in biotechnological industries [4–7].

In contrast to aerobic processes, where dissolved oxygen can be continuously measured, fermentative processes in anaerobic organisms pose a significant challenge due to the current insufficiency of control process technologies [6–10]. Commonly used pH detection in fermentation processes only reflects proton activity and is not sensitive to subtle changes in intracellular metabolism. Redox potential (ORP), or oxidation-reduction potential, captures electron transfers and reflects intracellular metabolism more accurately [6,11–15]. Recent advances in analytical technologies have facilitated the control and deciphering of complex bioconversion processes, with parameters such as pH, ORP, gas production rate, and flow rates routinely recorded in real-time [16–19].

Given the numerous applications of anaerobic biodigesters, it is crucial to develop strategies for engineering students to understand their operation and governing parameters across different contexts. This can be achieved through hands-on experience with the equipment or student-led experimental designs. The educational approach is grounded in theoretical psychological studies [5,7,8,20–24] highlighting the importance of appropriate teaching environments and the design and construction of equipment to reinforce learning.

In light of the significance of the anaerobic process and the need for continuous control, this study presents the design and fabrication of a laboratory-scale anaerobic batch biodigester, alongside its practical application involving brewer's yeast (*Saccharomyces cerevisiae*) in a semi-continuous control process. The results are subsequently compared with a previously proposed theoretical model [25–30]. The primary aim of this article is to demonstrate a laboratory-scale experimental design of an anaerobic biodigester and to propose user-friendly,

low-cost tools, software, and hardware. These resources will enable engineering students to develop autonomous control elements and transform the collected data into computer-interpretable parameters [31–34]. This research aims to connect the anaerobic digestion process in a sequentially loaded reactor on a laboratory scale, with a known microorganism and lab-prepared substrate, to the profiles of oxidation-reduction potential, pH, temperature, and absolute pressure [35–39].

Materials and Methods

Diagram of the Laboratory Reactor

The devised bioreactor (Figure 2.1) can be categorised into three distinct components: (1) Digestion system—encompassing the digester itself and elements in direct contact with it, such as sensors, heating cable, loading and unloading supplies, etc.; (3-6) Control system, circuits, and voltage source—responsible for receiving data and issuing commands essential for optimal system performance; and (7-8) Computer system, communication interface, and software [40–44].

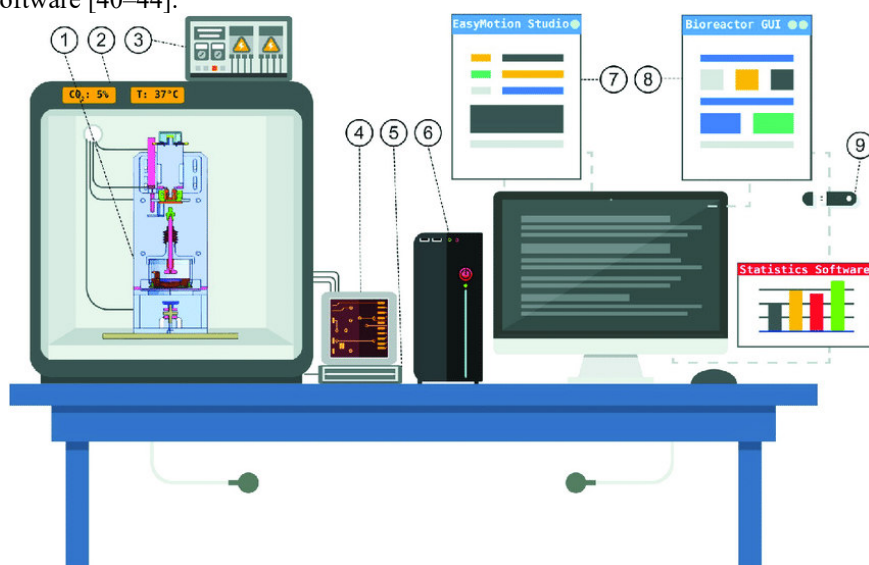


Figure 2.1. Basic diagram of experimental design.

2.1.1 Digestion System

The Digestion System comprises an insulated, hermetically sealed container featuring a feeding and evacuation system designed to ensure thorough mixing during each loading and unloading process. The container's upper section is equipped with an array of sensors, detailed as follows:

1. pH Sensor: A high-quality Scientific Grade Silver/Silver Chloride pH-10 sensor boasting a 95% response speed within one second.
2. ORP (Oxidation-Reduction Potential) Sensor (E): A premium sensor from Atlas Scientific [10,45–48] that utilises an integrated system and a simple serial communication protocol for instant E-value responses.
3. Absolute Pressure Sensor: The Phidgets mod. 1141-0—Gas Pressure Absolute Sensor, ranging from 15 to 115 kPa [49,50], is a high-level analog input sensor whose input is proportional to the ambient pressure.

For the calculation of the temperature from the analogical measurement, considering the resistive values depending on the temperature provided by the manufacturer, and with an algorithm in Scilab, we obtain Equation (2).

$$f(x) = 2.249 \times 10^{-5}x^2 + 0.06872x - 16.03 \quad (2)$$

Table 1. Characteristics of the thermistor NTC, Vishay.

Parameter		Value	Units
	Resistance value at 25 °C	10 K	Ω
	Tolerance of R25	± 3	%
	B25/85 (Beta)	3678	K
Temperatura range of operation		–5 to 105	°C

2.2 Preparation and Testing

2.2.1 Preparation of the Substrate

For the preparation of the substrate, the procedure described in bibliography was followed [4]. (1) The substrate was prepared, and its suitability checked. (2) The Brix level was measured and verified to be between 17 and 20 degrees. (3) Once this process was finished, 200 mL of the must was taken, and the yeast was added to it (approximately 2–4 g/L). Although an activation temperature of 37 °C is normally required, it was left at room temperature, as it has been previously proven that the inoculum is active under these conditions for working yeast.

2.2.2 Microbial Inoculum

Brewer's yeast was used whose species includes *Saccharomyces cerevisiae* with a yield of 0.25–0.33 kg of dry cell weight per kg of substrate.

2.2.3 Control and Saving Data

Through the Arduino (Appendix B shows the Arduino source code), the temperature was controlled and the signals from the pH, ORP, absolute pressure, and temperature sensors (inside the digester and outside the environment) were read. Data were sent to the computer where they were stored by means of the use of Processing tool. Shown in Appendix C is the Processing source code, and Figure 6 displays the interface. Once all the information was entered, it was saved in a file on the computer's hard disk.

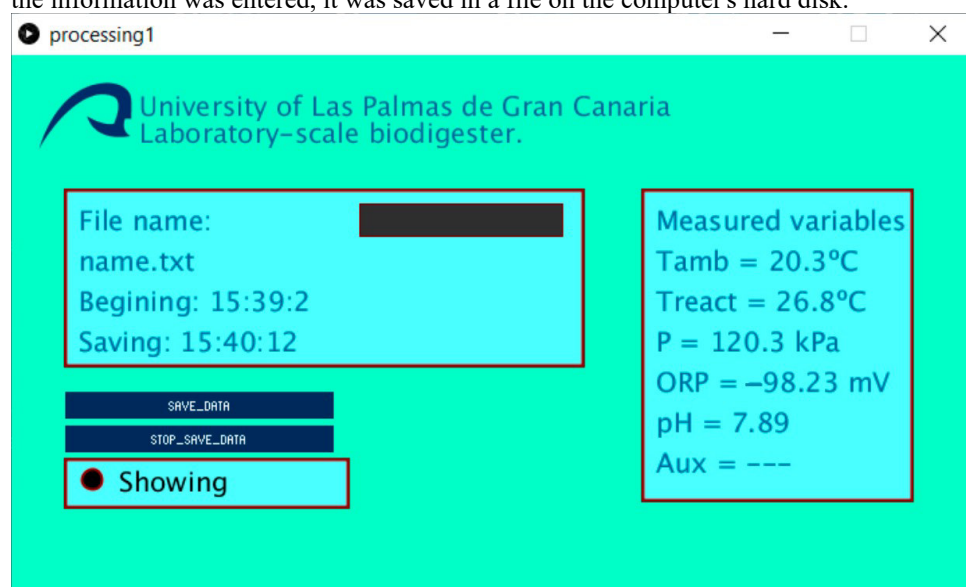


Figure 2.2. Processing PC interface data logger.

3. Results

a. Digestion Model

Dynamic simulation between reality and model is a very important way for research, as it enables to provide strategies for the An average representation of the tests, carried out in the biodigester over 5 weeks, is shown in Table 2. The data was processed using a computerised tool from Scilab. Scilab is a software for numerical analysis, with a high-level programming language for scientific calculation. With the obtained data, a series of graphs were elaborated and the most relevant ones are presented in Figures 8–10.

Table 2. Laboratory-scale biodigester; performance periods, operating volume, and Brix measures.

Stage	Date	Feeding/Evacuation (mL)	Brix Grades			Remarks
			1st Lecture	2nd Lecture	Average	
1	13 June	300	20.30			
2	18 June	75	20.31	20.29	20.30	
3	23 June	50	20.33	20.24	20.26	Addition NaOH (↑alkalinity)

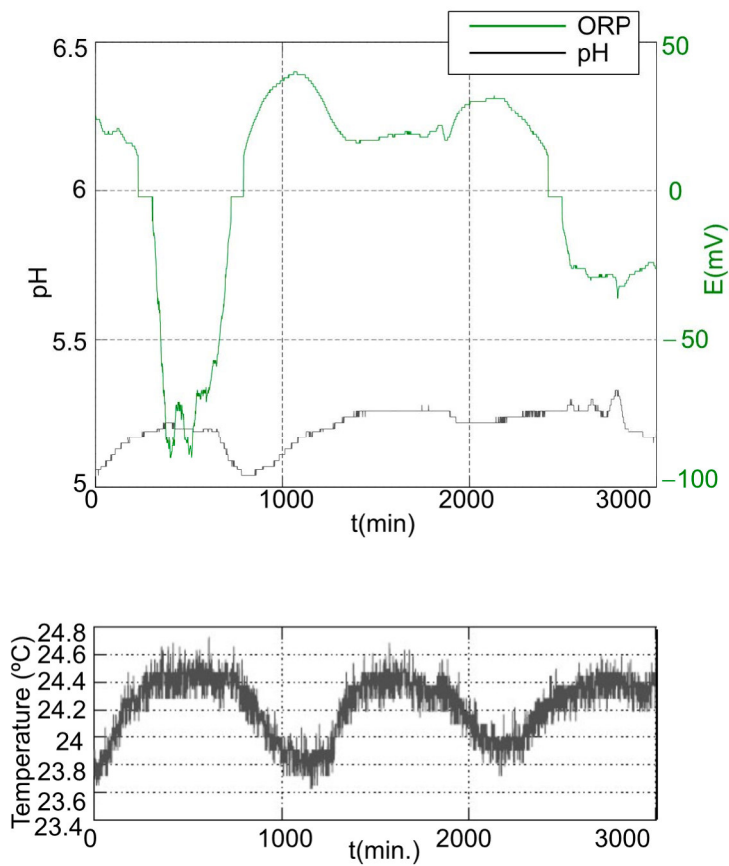


Figure 3.1 ORP, pH, and temperature in the second period.

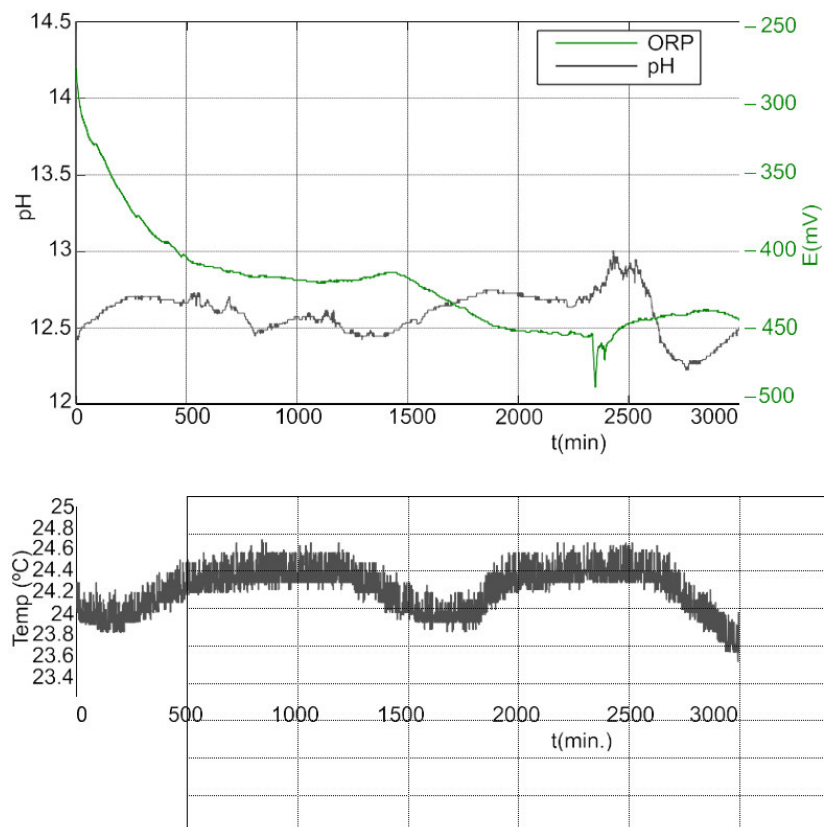


Figure 3.2. ORP, pH, and temperature in the third period.

4. Conclusions

The developed anaerobic bioreactor monitoring system demonstrates effective performance for small-scale testing, serving as a valuable resource for research and education. It facilitates the development of new research projects while supporting engineering students' learning. The continuous data collection by ORP, pH, temperature, and pressure sensors allows for easy determination of factors influencing anaerobic microorganism growth. Subsequent data processing enables the creation of graphs that can be compared with a previously proposed theoretical model and relevant governing equations (e.g., Nernst equation). A notable advantage of this design is its reliance on flexible, easily accessible, and open-source software, which allows students to adapt the experimental design to specific cases. The results indicate that the experimental setup is viable for controlling and collecting data on growth-related magnitudes of anaerobic bacteria within a digester. In conclusion, the economically feasible design and construction of a laboratory-scale bioreactor is a readily available tool for engineering students to enhance their knowledge and learning experience.

Acknowledgements: This research has been funded by TETFUND, Nigeria. We are immensely grateful.

Conflicts of Interest: The authors declare no conflict of interest.

Appendix A SCILAB Source Code

```
clear; clc; mu_max=.1/3600;
k_s=100; k_d=.00001; k_x=.00000150; V_1=.01; V_2=3.99; V_T=V_1+V_2;
S_min=k_d*k_s/(mu_max-k_d); S_in=130; dt=100; time=200*24*3600; Delta_t=.05*24*3600;
q=round(Delta_t/dt);
t=0:dt:time;
X=zeros(1,length(t)); S=zeros(1,length(t)); X(1)=.1; S(1)=0; S_in=S_in; X_in=.1;
e=1; f=0; g=0;
for k=2:length(t)
f=f+1;
if f>=q //Impulse input
S(k-1)=(V_2*S(k-1)+V_1*S_in)/V_T; X(k-1)=(V_2*X(k-1)+V_1*X_in)/V_T; f=0;
end
//Prediction step.
X(k)=(1+(mu_max*S(k-1)/(k_s+S(k-1))-k_d)*dt)*X(k-1);
S(k)=(1-k_x*X(k-1)/(k_s+S(k-1))*dt)*S(k-1);

//Initialization and recursive correction steps. While (e>=.01)
x=X(k);
s=S(k);
X(k)=X(k-1)+dt/2*((mu_max*S(k-1)/(k_s+S(k-1))-k_d)*X(k-1)+
(mu_max*S(k)/(k_s+S(k))-k_d)*X(k));
S(k)=S(k-1)-k_x*dt/2*(S(k-1)/(k_s+S(k-1))*X(k-1)+S(k)/(k_s+S(k))*X(k)); e=sqrt((x-X(k))^2+(s-S(k))^2);
end
end
```

Appendix B Microcontroller Source Code (Arduino)

```
// ****Digital inputs for pH y ORP****
#include <SoftwareSerial.h> //add the soft serial library #define rxph 4 //set theRX pin to pin 2
#define txph 5 //set the TX pin to pin 3 #define rxorp 2#define txorp 3
// ****pH data***
SoftwareSerial phserial(rxph, txph); //enable the soft serial port
String inputstringph = ""; // string to hold incoming data from the PC
String sensorstringph = ""; //a string to hold the data from the Atlas Scientific product boolean
input_stringcompleteph = false; //have we received all the data from the PC boolean sensor_stringcompleteph =
false; //have we received all the data from the Atlas Scientific product
// ****ORP data***
SoftwareSerial orpserial(rxorp, txorp);
String inputstringorp = ""; //a string to hold incoming data from the PC
String sensorstringorp = ""; //a string to hold the data from the Atlas Scientific product boolean
input_stringcompleteorp = false; //have we received all the data from the PC boolean sensor_stringcompleteorp =
false; //have we received all the data from the Atlas Scientific product
// ****Analog inputs***
String sensorpresion=""; //presion
```

```
float ntc_biodig=0; //termistor NTC lectura sistema de control float ntc_ext=0; //termistor NTC lectura entorno
int analogPin1 = A1; //definimos los pines de entrada para la temperatura entorno int analogPin2 =
A2; //definimos los pines de entrada para la temperatura sistema
// **** SETUP ****
void setup() { //set up the hardware

Serial.begin(9600);
phserial.begin(9600); //set baud rate for software serial port to 38400 orpserial.begin(9600);
phserial.print("\r\n");
orpserial.print("\r\n"); phserial.print("\r\n"); orpserial.print("\r\n");
inputstringph.reserve(5); //set aside some bytes for receiving data from the PC

sensorstringph.reserve(30); //set aside some bytes for receiving data from Atlas Scientific product

inputstringorp.reserve(5); //set aside some bytes for receiving data from the PC sensorstringorp.reserve(30);
pinMode(analogPin1, INPUT); //def de los pines de entrada

}
archivo.flush(); // Writes the remaining data to the file archivo.close(); // Finishes the file
nom_archivo="name.txt";
}
```

References

1. Brito-Espino, S.; Ramos-Martín, A.; Pérez-Báez, S.O.; Mendieta-Pino, C.; Leon-Zerpa, F. A Framework Based on Finite Element Method (FEM) for Modelling and Assessing the Affection of the Local Thermal Weather Factors on the Performance of Anaerobic Lagoons for the Natural Treatment of Swine Wastewater. *Water* **2021**, *13*, 882. [CrossRef]
2. Cano, E.; Ruiz, J.G.; Garcia, I.A. Integrating a learning constructionist environment and the instructional design approach into the definition of a basic course for embedded systems design. *Comput. Appl. Eng. Educ.* **2015**, *23*, 36–53. [CrossRef]
3. Garcia, I.A.; Cano, E.M. Designing and implementing a constructionist approach for improving the teaching-learning process in the embedded systems and wireless communications areas. *Comput. Appl. Eng. Educ.* **2014**, *22*, 481–493. [CrossRef]
4. Available online: <http://www.atago.net/Spanish/download.htmlRX-7000i> (accessed on 11 June 2021).
5. Refractómetro Digital Automático Atago. Available online: <http://www.atago.net/Spanish/download.html> (accessed on 14 June 2021).
6. Jagnow, G.; Dawind, W. *Biotechnología: Introducción Con Experimentos Modelo*; Acribia S.A.: Zaragoza, Spain, 1991.
7. Liu, C.-G.; Xue, C.; Lin, Y.-H.; Bai, F.-W. Redox potential control and applications in microaerobic and anaerobic fermentations. *Biotechnol. Adv.* **2013**, *31*, 257–265. [CrossRef]
8. Madsen, M.; Holm-Nielsen, J.B.; Esbensen, K.H. Monitoring of anaerobic digestion processes: A review perspective. *Renew. Sustain. Energy Rev.* **2011**, *15*, 3141–3155. [CrossRef]
9. Mekic, E.; Djokic, I.; Zejnelagic, S.; Matovic, A. Constructive approach in teaching of voip in line with good laboratory and manufacturing practice. *Comput. Appl. Eng. Educ.* **2016**, *24*, 277–287. [CrossRef]
10. Pantaleo, A.; De Gennaro, B.; Shah, N. Assessment of optimal size of anaerobic co-digestion plants: An application to cattle farms in the province of Bari (Italy). *Renew. Sustain. Energy Rev.* **2013**, *20*, 57–70. [CrossRef]
11. Atlas Scientific. Atlas Scientific. Orpatlas. Available online: https://atlas-scientific.com/?gclid=EAIaIQobChMIvbPk8o3Z8gIVied3Ch03AgqaEAAAYASAAEgKLzPD_BwE (accessed on 19 July 2021).
12. Sorathia, K.; Servidio, R. Learning and experience: Teaching tangible interaction & edutainment. *Procedia—Soc. Behav. Sci.* **2012**, *64*, 265–274.
13. Taylhardat Arjona, L.A. *El biogas. Fundamentos e Infraestructura Rural*; Instituto de Ingenieria Agrícola; Facultad de Agronomía U.C.V: Maracay, Venezuela, 1986.
14. Leon, F.; Ramos, A.; Vaswani, J.; Mendieta, C.; Brito, S. Climate Change Mitigation Strategy through Membranes Replacement and Determination Methodology of Carbon Footprint in Reverse Osmosis RO Desalination Plants for Islands and Isolated Territories. *Water* **2021**, *13*, 293. [CrossRef]
15. Products for USB Sensing and Control. Products for Usb Sensing and Control. Available online: www.phidgets.com (accessed on 1 July 2021).

16. Parralejo, A.; Royano, L.; González, J.; González, J. Small scale biogas production with animal excrement and agricultural residues. *Ind. Crops Prod.* **2019**, *131*, 307–314. [CrossRef]
17. Holm-Nielsen, J.; Seadi, T.A.; Oleskowicz-Popiel, P. The future of anaerobic digestion and biogas utilisation. *Bioresour. Technol.* **2009**, *100*, 5478–5484. [CrossRef]
18. Park, J.H.; Park, J.H.; Lee, S.H.; Jung, S.P.; Kim, S.H. Enhancing anaerobic digestion for rural wastewater treatment with granular activated carbon (GAC) supplementation. *Bioresour. Technol.* **2020**, *315*, 123890. [CrossRef] [PubMed]
19. Jiang, Y.; Bebee, B.; Mendoza, A.; Robinson, A.K.; Zhang, X.; Rosso, D. Energy footprint and carbon emission reduction using off-the-grid solar-powered mixing for lagoon treatment. *J. Environ. Manag.* **2018**, *205*, 125–133. [CrossRef] [PubMed]
20. Duan, N.; Zhang, D.; Khoshnevisan, B.; Kougias, P.G.; Treu, L.; Liu, Z.; Lin, C.; Liu, H.; Zhang, Y.; Angelidaki, I. Human waste anaerobic digestion as a promising low-carbon strategy: Operating performance, microbial dynamics and environmental footprint. *J. Clean. Prod.* **2020**, *256*, 120414. [CrossRef]
21. Mendieta-Pino, C.A.; Ramos-Martin, A.; Perez-Baez, S.O.; Brito-Espino, S. Management of slurry in Gran Canaria Island with full-scale natural treatment systems for wastewater (NTSW). One year experience in livestock farms. *J. Environ. Manag.* **2019**, *232*, 666–678.
22. Muga, H.; Mihelcic, J. Sustainability of wastewater treatment technologies. *J. Environ. Manag.* **2008**, *88*, 437–447. [CrossRef]
23. Wu, B.; Chen, Z. An integrated physical and biological model for anaerobic lagoons. *Bioresour. Technol.* **2011**, *102*, 5032–5038. [CrossRef] [PubMed]
24. Wu, B. Advances in the use of CFD to characterise, design and optimise bioenergy systems. *Comput. Electron. Agric.* **2013**, *93*, 195–208. [CrossRef]
25. Donoso-Bravo, A.; Sadino-Riquelme, C.; Gómez, D.; Segura, C.; Valdebenito, E.; Hansen, F. Modelling of an anaerobic plug-flow reactor. Process analysis and evaluation approaches with non-ideal mixing considerations. *Bioresour. Technol.* **2018**, *260*, 95–104.
26. Rajeshwari, K.; Balakrishnan, M.; Kansal, A.; Lata, K.; Kishore, V. State-of-the-art of anaerobic digestion technology for industrial wastewater treatment. *Renew. Sustain. Energy Rev.* **2000**, *4*, 135–156. [CrossRef]
27. Lauwers, J.; Appels, L.; Thompson, I.P.; Degreève, J.; Impe, J.F.V.; Dewil, R. Mathematical modelling of anaerobic digestion of biomass and waste: Power and limitations. *Prog. Energy Combust.* **2013**, *39*, 383–402. [CrossRef]
28. Wade, M.; Harmand, J.; Benyahia, B.; Bouchez, T.; Chaillou, S.; Cloez, B. Perspectives in mathematical modelling for microbial ecology. *Ecol. Model.* **2016**, *321*, 64–74. [CrossRef]
29. Batstone, D.; Keller, J.; Angelidaki, I.; Kalyuzhnyi, S.; Pavlostathis, S.; Rozzi, A.; Sanders, W.; Siegrist, H.; Vavilin, V. The IWAAnaerobic Digestion Model No 1 (ADM1). *Water Sci. Technol.* **2002**, *45*, 65–73. Available online: <https://library.lanl.gov/cgi-bin/getfile?00285556.pdf> (accessed on 1 September 2020). [CrossRef]
30. Kleerebezem, R.; van Loosdrecht, M.C.M. Critical analysis of some concepts proposed in ADM1. *Water Sci. Technol.* **2006**, *54*, 51–57. [CrossRef] [PubMed]
31. Li, D.; Lee, I.; Kim, H. Application of the linearised ADM1 (LADM) to lab-scale anaerobic digestion system. *J. Environ. Chem. Eng.* **2021**, *9*, 105193. [CrossRef]
32. Fleming, J.G. Novel Simulation of Anaerobic Digestion Using Computational Fluid Dynamics. Ph.D. Thesis, North Carolina State University, Raleigh, NC, USA, 2002.
33. Goodarzi, D.; Sookhak Lari, K.; Mossaiby, F. Thermal effects on the hydraulic performance of sedimentation ponds. *J. Water Process. Eng.* **2020**, *33*, 101100. [CrossRef]
34. Brito-Espino, S.; Ramos-Martín, A.; Pérez-Báez, S.; Mendieta-Pino, C. Application of a mathematical model to predict simultaneous reactions in anaerobic plug-flow reactors as a primary treatment for constructed wetlands. *Sci. Total Environ.* **2020**, *713*, 136244. [CrossRef]
35. Mahmudul, H.; Rasul, M.; Akbar, D.; Narayanan, R.; Mofijur, M. A comprehensive review of the recent development and challenges of a solar-assisted biodigester system. *Sci. Total Environ.* **2021**, *753*, 141920. [CrossRef] [PubMed]
36. Atelge, M.; Atabani, A.; Banu, J.R.; Krisa, D.; Kaya, M.; Eskicioglu, C.; Kumar, G.; Lee, C.; Yildiz, Y.; Unalan, S.; et al. A critical review of pretreatment technologies to enhance anaerobic digestion and energy recovery. *Fuel* **2020**, *270*, 117494. [CrossRef]
37. Tumilar, A.S.; Milani, D.; Cohn, Z.; Florin, N.; Abbas, A. A Modelling Framework for the Conceptual Design of Low-Emission Eco-Industrial Parks in the Circular Economy: A Case for Algae-Centered Business Consortia. *Water* **2021**, *13*, 69. [CrossRef]
38. Haßler, S.; Ranno, A.M.; Behr, M. Finite-element formulation for advection–reaction equations with change of variable and discontinuity capturing. *Comput. Methods Appl. Mech. Eng.* **2020**, *369*, 113171. [CrossRef]

39. Mirza, I.A.; Akram, M.S.; Shah, N.A.; Imtiaz, W.; Chung, J.D. Analytical solutions to the advection-diffusion equation with Atangana-Baleanu time-fractional derivative and a concentrated loading. *Alex. Eng. J.* **2021**, *60*, 1199–1208. [CrossRef]
40. Singh, S.; Bansal, D.; Kaur, G.; Sircar, S. Implicit-explicit-compact methods for advection diffusion reaction equations. *Comput. Fluids* **2020**, *212*, 104709. [CrossRef]
41. Zeng, L.; Chen, G. Ecological degradation and hydraulic dispersion of contaminant in wetland. *Ecol. Model.* **2011**, *222*, 293–300. [CrossRef]
42. Bozkurt, S.; Moreno, L.; Neretnieks, I. Long-term processes in waste deposits. *Sci. Total Environ.* **2000**, *250*, 101–121. [CrossRef]
43. Song, L.; Li, P.W.; Gu, Y.; Fan, C.M. Generalised finite difference method for solving stationary 2D and 3D Stokes equations with a mixed boundary condition. *Comput. Math. Appl.* **2020**, *80*, 1726–1743. [CrossRef]
44. Ukai, S. A solution formula for the Stokes equation in R_n^+ . *Commun. Pure Appl. Math.* **1987**, *40*, 611–621. [CrossRef]
45. Reddy, J.; Gartling, D. *The Finite Element Method in Heat Transfer and Fluid Dynamics*, 3rd ed.; CRC Press: Boca Raton, FL, USA, 2010; pp. 1–483.
46. Alvarez-Hostos, J.C.; Bencomo, A.D.; Puchi-Cabrera, E.S.; Fachinotti, V.D.; Tourn, B.; Salazar-Bove, J.C. Implementation of a standard stream-upwind stabilisation scheme in the element-free Galerkin based solution of advection-dominated heat transfer problems during solidification in direct chill casting processes. *Eng. Anal. Bound. Elem.* **2019**, *106*, 170–181. [CrossRef]
47. Guldentops, G.; Van Dessel, S. A numerical and experimental study of a cellular passive solar façade system for building thermal control. *Sol. Energy* **2017**, *149*, 102–113. [CrossRef]
48. Lawrence, M.G. The Relationship between Relative Humidity and the Dewpoint Temperature in Moist Air: A Simple Conversion and Applications. *Bull. Am. Meteorol. Soc.* **2005**, *86*, 225–234. [CrossRef]
49. Çengel, Y. Heat Transfer: A Practical Approach. In *McGraw-Hill Series in Mechanical Engineering*; McGraw Hill Books: London, UK, 2003.
50. Walton, G.N. *Thermal Analysis Research Program Reference Manual*; NBSIR, Department of Energy, Office of Building Energy Research and Development: Washington, DC, USA, 1983.
51. Monod, J. The Growth of Bacterial Cultures. *Annu. Rev. Microbiol.* **1949**, *3*, 371–394. [CrossRef]
52. Rosso, L.; Lobry, J.; Flandrois, J. An Unexpected Correlation between Cardinal Temperatures of Microbial Growth Highlighted by a New Model. *J. Theor. Biol.* **1993**, *162*, 447–463. [CrossRef] [PubMed]
53. Herus, V.A.; Ivanchuk, N.V.; Martyniuk, P.M. A System Approach to Mathematical and Computer Modeling of Geomigration Processes Using Freefem++ and Parallelization of Computations. *Cybern Syst. Anal.* **2018**, *54*, 284–292. [CrossRef]
54. Donoso-Bravo, A.; Bandara, W.; Satoh, H.; Ruiz-Filippi, G. Explicit temperature-based model for anaerobic digestion: Application in domestic wastewater treatment in a UASB reactor. *Bioresour. Technol.* **2013**, *133*, 437–442. [CrossRef]
55. Donoso-Bravo, A.; Retamal, C.; Carballa, M.; Ruiz-Filippi, G.; Chamy, R. Influence of temperature on the hydrolysis, acidogenesis and methanogenesis in mesophilic anaerobic digestion: Parameter identification and modeling application. *Water Sci. Technol.* **2009**, *60*, 9–17. [CrossRef]
56. Wang, R.; Lv, N.; Li, C.; Cai, G.; Pan, X.; Li, Y.; Zhu, G. Novel strategy for enhancing acetic and formic acids generation in acidogenesis of anaerobic digestion via targeted adjusting environmental niches. *Water Res.* **2021**, *193*, 116896. Available online: <https://www.sciencedirect.com/science/article/pii/S0043135421000944>(accessed on 23 June 2021). [CrossRef]
57. Weißbach, M.; Drewes, J.E.; Koch, K. Application of the oxidation reduction potential (ORP) for process control and monitoring nitrite in a Coupled Aerobic-anoxic Nitrous Decomposition Operation (CANDO). *Chem. Eng. J.* **2018**, *343*, 484–491. Available online: <https://www.sciencedirect.com/science/article/pii/S1385894718303929>(accessed on 30 June 2021). [CrossRef]
58. Ao, T.; Chen, L.; Zhou, P.; Liu, X.; Li, D. The role of oxidation-reduction potential as an early warning indicator, and a microbial instability mechanism in a pilot-scale anaerobic mesophilic digestion of chicken manure. *Renew. Energy* **2021**, *179*, 223–232. Available online: <https://www.sciencedirect.com/science/article/pii/S0960148121010521>(accessed on 1 July 2021). [CrossRef]